# **COMBINED HEAT AND POWER SUSTAINABILITY + ROI**:

#### **Powering the Future**



Sink 1922

A Caterpillar Company

#### EDWARD STOERMER COGEN SALES LEAD

#### CRAIG PLEIMAN SALES ENGINEER

#### **Powering the Future**





A Caterpillar Company



#### **INTRODUCTIONS:** LATHROP TROTTER / KOCH APPLIED

**EDWARD STOERMER:** 

**CRAIG PLEIMAN:** 

**SOLAR GAS TURBINES (CATERPILLAR CO)** 



#### **GAS TURBINE BASICS (5 MIN)** 1

2. COMBINED HEAT AND POWER (CHP) BASICS (5 MIN)

3. HEAT SINKS THE 1 THING TO REMEMBER

4. DRIVERS: ECONOMICS+RELIABILITY+SUSTAINABILITY

5. WHERE IT APPLIES

- 6. SIZE AND SELECTION OF GAS TURBINE (GT) & HEAT RECOVERY STEAM GENERATOR (HRSG)
- 7. TYPICAL PRELIMINARY CHP REPORT
- 8. SEIZE THE OPPORTUNITY

- 10. GREEN HYDROGEN.
- 11. Q&A SESSION





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#### GAS TURBINES

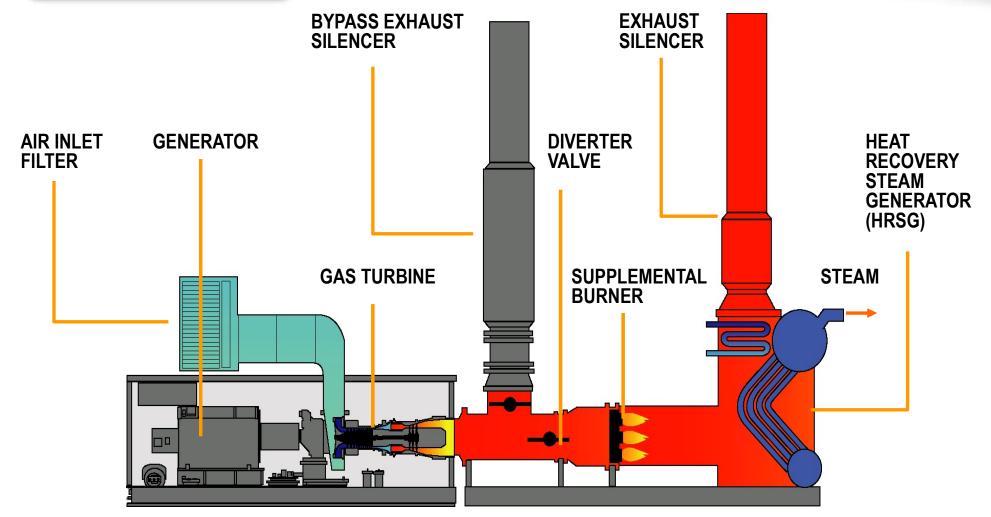
- Steam generation 20,000 PPH AND >
- Larger capacities 4MW >
- RECIPROCATING ENGINES
  - Quicker starts
  - Higher fuel to power efficiency, but less heat output.
  - Hot water heat sinks are best

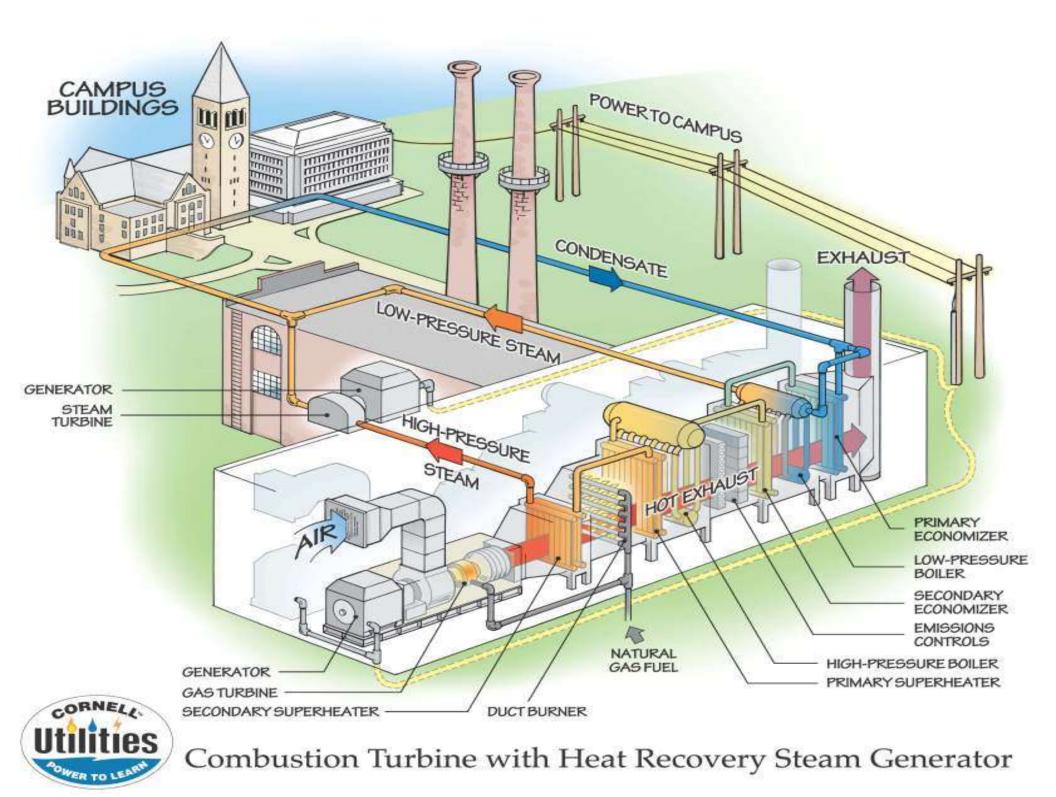
#### STEAM TURBINES

- Larger steam systems that use multiple pressures
- Backpressure STG's can be lowest cost in \$/kw.









**COMBINED HEAT & POWER : CHP / CO-GENERATION** 

# CHP: Use one fuel source to produce two types of useful energy.

### **1. ELECTRICAL POWER**



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**COMBINED HEAT & POWER : CHP / CO-GENERATION** 

# CHP: Use one fuel source to produce two types of useful energy.

## 1. USEFUL HEAT (STEAM)



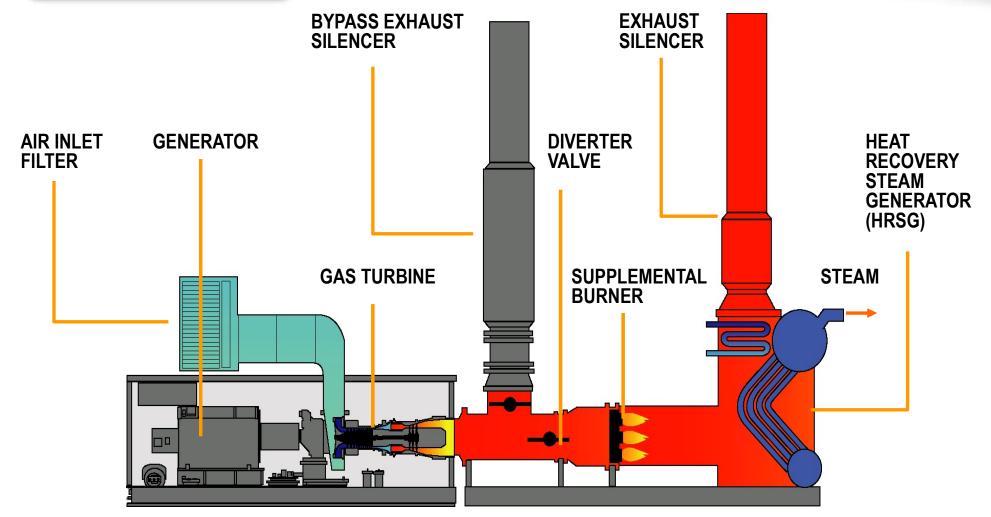
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#### **COMBINED HEAT & POWER : CHP / CO-GENERATION**

**FUELS**: NATURAL GAS DIGESTER GAS LANDFILL GAS **RENEWABLE NAT GAS HYDROGEN (%)** LIQUID FUELS: #2 Oil **"OPPORTUNITY" FUELS** 







#### **HIGHER EDUCATION: ENERGY STAR**

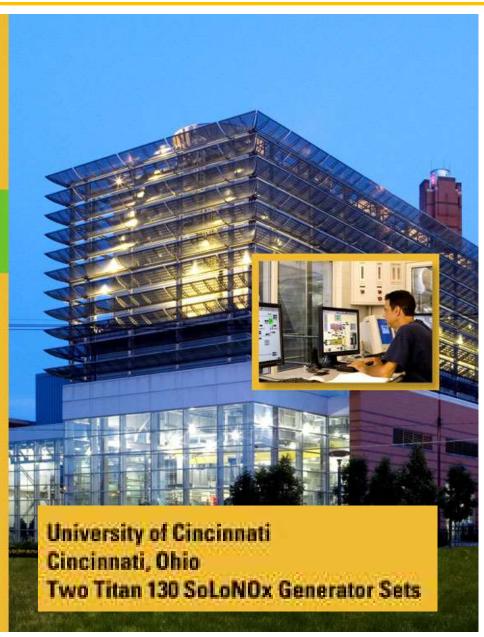
#### EFFICIENT. RELIABLE. RESPONSIBLE. COMBINED HEAT AND POWER

CO2 Emissions Reduction Equivalent to Planting 4300 Acres of Forest

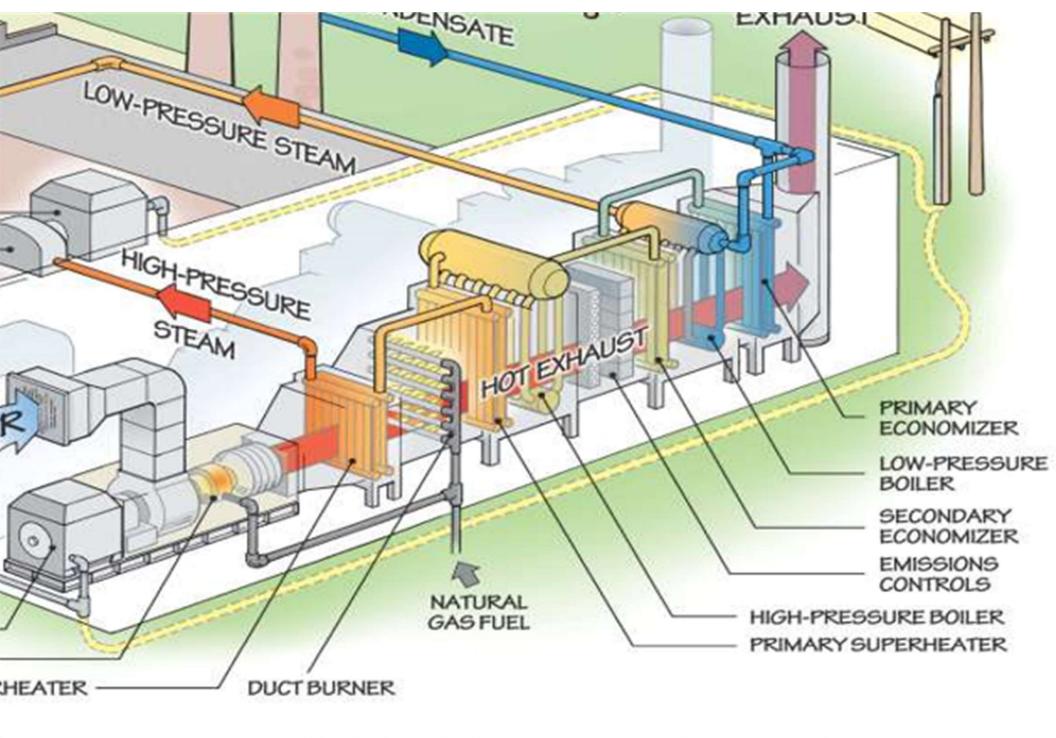


University of Cincinnati Cincinnati, Ohio Two Titan 130 SoLoNOx Generator Sets









on Turbine with Heat Recovery Steam Generator

#### **NATURAL GAS & REFINERY GAS**







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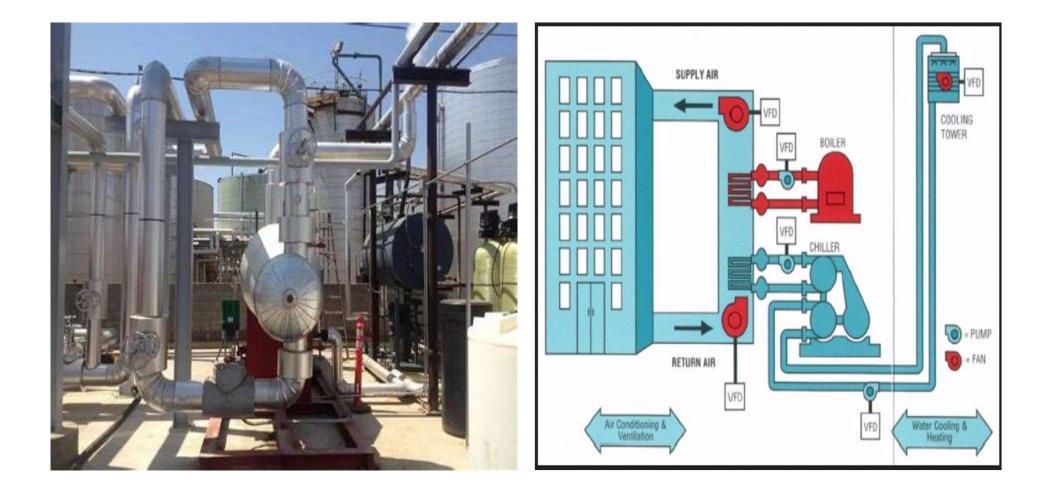
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#### **INDUSTRIAL AND COMMERCIAL HEATING SYSTEMS**





#### WHERE WE HAVE SUFFICIENT THERMAL (STEAM) LOADS





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#### **TYPICAL "HEAT SINKS" OR STEAM USERS**

- Dairies
- Chemical Plants
- Food and Beverage
- Hospitals
- Refining
- Pharmaceuticals
- Campus
- Microgrids

- Cooking / Sterilization
- Process Heat
- Sterilization / Process
- HVAC / Sterilization
- Process
- Process and HVAC
- District Steam Heating
- Heating for the Grid

#### SMALL POWER PRODUCERS CAN BE MORE EFFICIENT THAN LARGE POWER PRODUCERS !!

#### Small Scale Power (CHP) Project

#### Utility Scale Power Producer







#### WHAT CHP IS NOT:

#### SMALL POWER PRODUCERS CAN BE MORE EFFICIENT THAN LARGE POWER PRODUCERS IF THEY RECOVER AND USE THE THERMAL ENERGY

#### Small Scale Power (CHP) Project

#### Utility Scale Power Producer





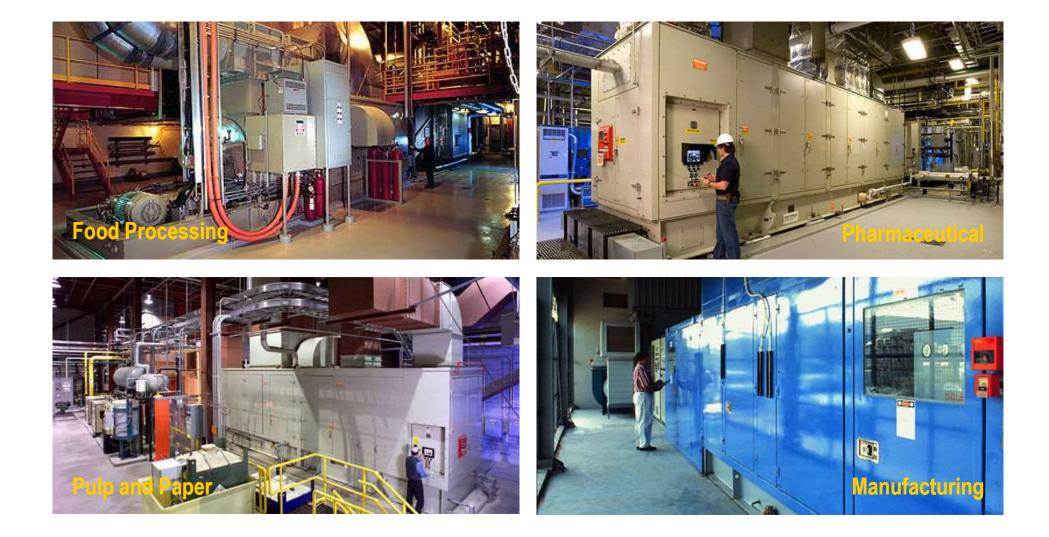
Without CHP	ENERGY	ENERGY USAGE	ENERGY USAGE, MW	ENERGY INPUT, MW	SYSTEM EFFICIENCY
	Thermal	36 000 lbs/hr	10.7	13.1	82%
	Electrical	5 460 kW	5.5	15.6	35%
	Total		16.2	28.7	56%
With CHP	Thermal	36 000 lbs/hr	10.7	20.1	-
	Electrical	5 460 kW	5.5		-
Ň	Total		16.2	20.1	80.5%

#### **43% Improvement in Efficiency**



#### WHERE DOES CHP APPLY

#### **INDUSTRIES USING CHP**





#### **DRIVERS: THEN AND NOW**

- A decade ago, the drivers were:
- Almost Exclusively Economics
- Now the drivers are:
- Economics +
- Sustainability Corporate Goals +
- Reliability & Resiliency + Future Flexibility (Fuels)



#### SUSTAINABILITY

#### **OPERATIONS**



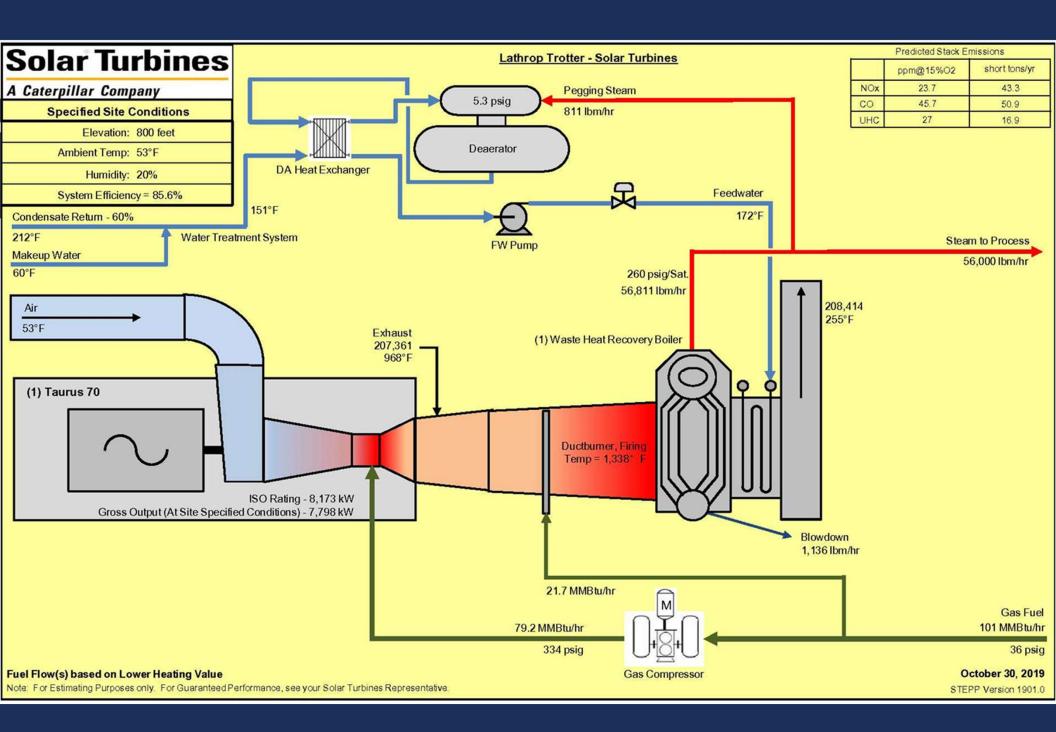
#### FINANCIAL

GOALS	HOW CHP MEETS GOALS
REDUCE <b>EMISSIONS</b> & ACHIEVE GOALS 30-50% (Typical)	EFFICIENCY & CLEAN FUELS
IMPROVE <b>RELIABILITY</b> & REDUCE OPERATING EXPENSE	REDUNDANCY & RELIABILITY IMPROVEMENTS. REDUCE ENERGY COSTS
REDUCE PER UNIT COST OF PRODUCTION	REDUCE ENERGY RQUIRED PER UNIT PRODUCED
IMPROVE FORCASTING ACCURACY EFFICIENT USE OF CAPITOL	FUEL COST STABILITY & PREDICTABILITY OF NATURAL GAS vs ELECTRICAL POWER
GOOD NEIGHBOR	PATH WAY to ZERO CARBON EMISSIONS
	REDUCE EMISSIONS & ACHIEVE GOALS 30-50% (Typical) IMPROVE RELIABILITY & REDUCE OPERATING EXPENSE REDUCE PER UNIT COST OF PRODUCTION IMPROVE FORCASTING ACCURACY EFFICIENT USE OF CAPITOL

## SUSTAINABILITY

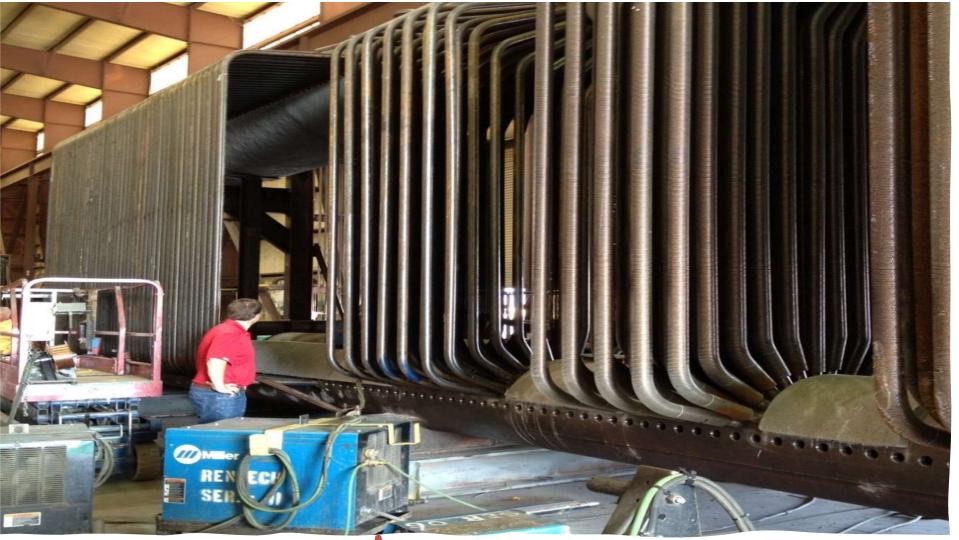
### FINANCIAL

## **OPERATIONS**









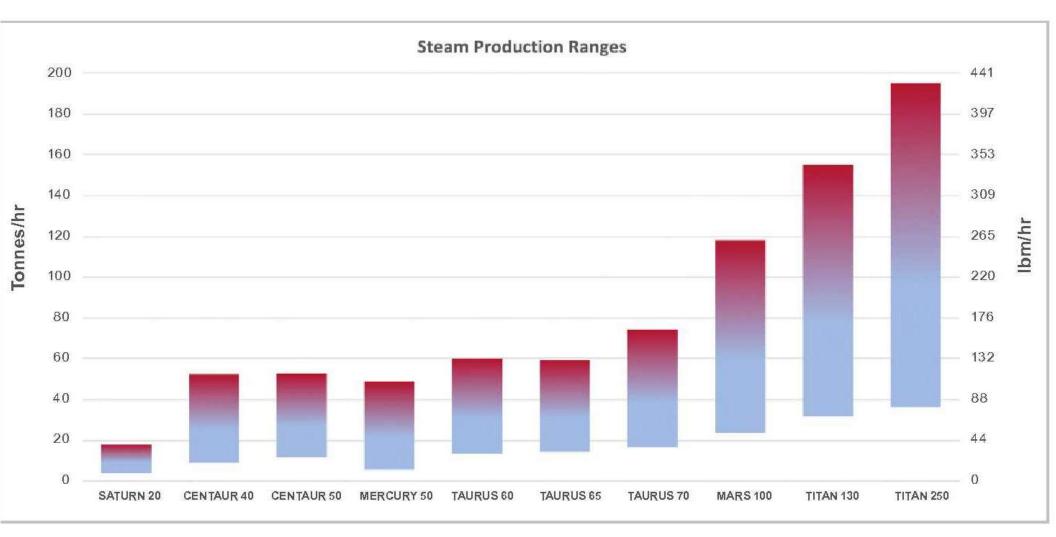
## WATER TUBE STYLE HEAT RECOVERY STEAM GENERATOR

TO RECOVER THE EXHAUSTED ENERGY FROM THE GAS TURBINE THESE HRSG'S CONVERT THE HOT GASES TO USEABLE STEAM FOR THE PLANT / PROCESS OR CAMPUS FOR HEATING.

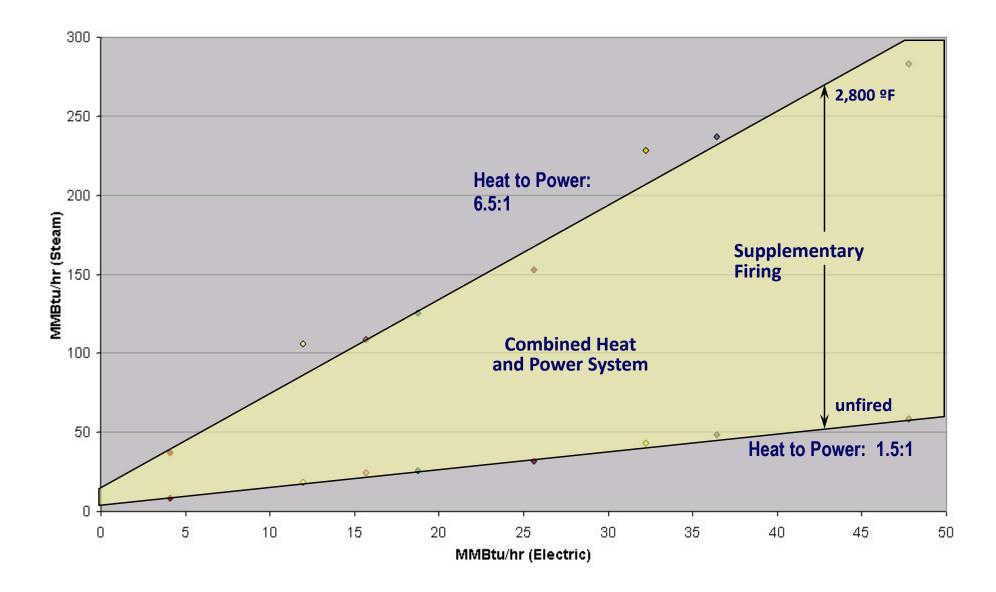


## Duct Burner

# **COMBINED HEAT AND POWER PERFORMANCE**



# HEAT / POWER RATIOS FOR CHP









The results generated by the CHP Emissions Calculator are intended for educational and outreach purposes only; it is not designed for use in developing emission inventories or preparing air permit applications.

Annual Emissions Analysis					
	CHP System	Displaced Electricity Production	Displaced Thermal Production	Emissions/Fuel Reduction	Percent Reduction
NOx (tons/year)	43.51	78.92	44.50	79.90	65%
SO2 (tons/year)	1.66	150.70	0.22	149.27	99%
CO2 (metric tons/year)	83,973	112,520	48,035	76,583	48%
Carbon (metric tons/vear)	22,902	30.687	13,100	20.886	48%
Fuel Consumption (MMBtu/year)	1,555,699	1,341,814	889,908	676,023	30%
Acres of Forest Equivalent				20,886	
Number of Cars Removed				13,054	

Displaced Electricity Generation Profile: eGRID State Average Fossil 2016

**Region Selected: Ohio** 

This reduction is equal to removing the carbon that would be absorbed by 20,886 acres of forest



This reduction is equal to removing the carbon emissions from 13,054 cars



## **Solar Turbines**

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Solar Turbines - Lathrop Trotter

**Midwest USA** 

**Project Description:** 

(1) Taurus 70-11101S Axial with fired HRSG and SCR Emission Control System

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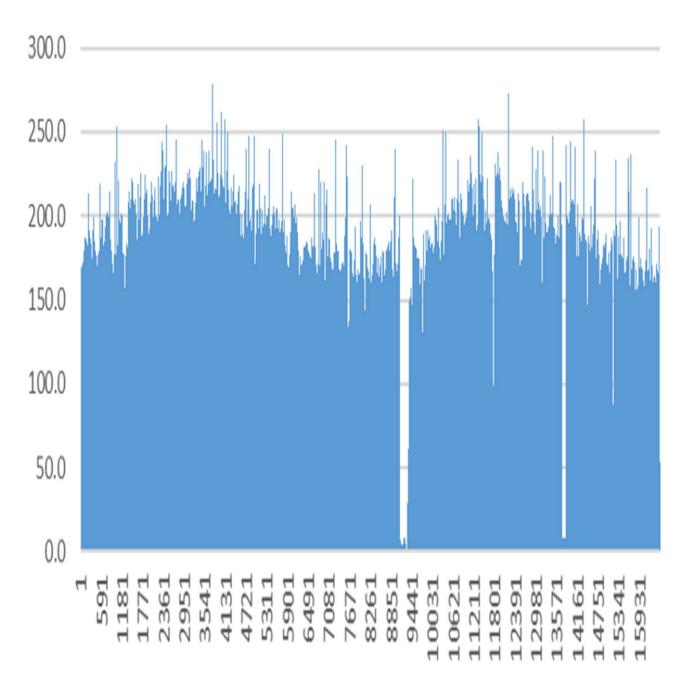
- 7. TYPICAL PRELIMINARY CHP REPORT
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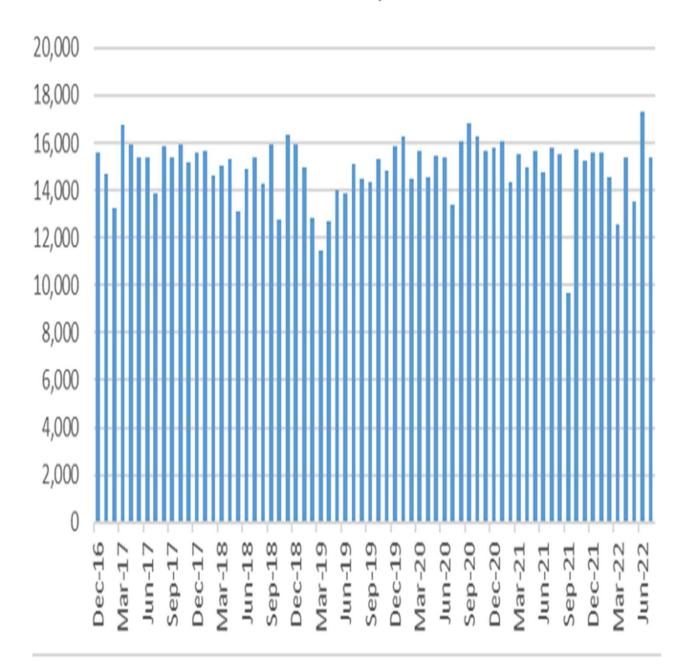
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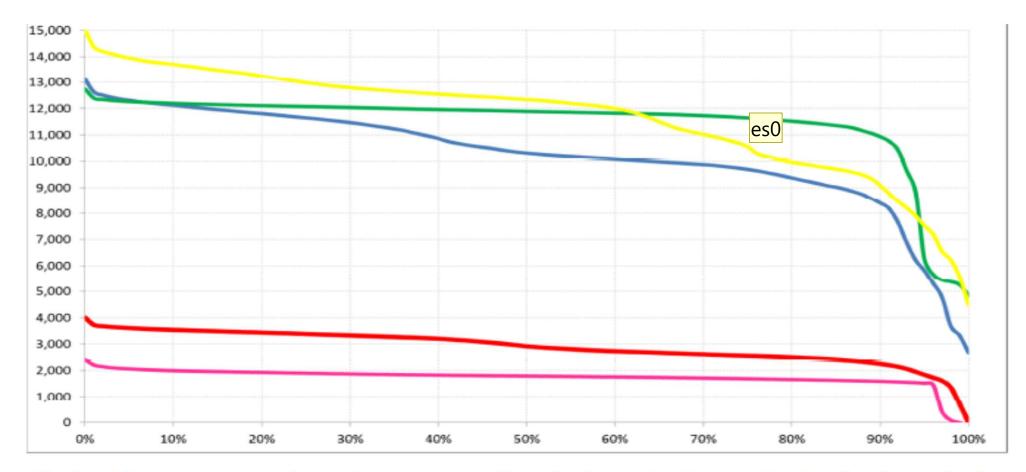
# Hourly Steam Flow







## **Load Duration Curves**

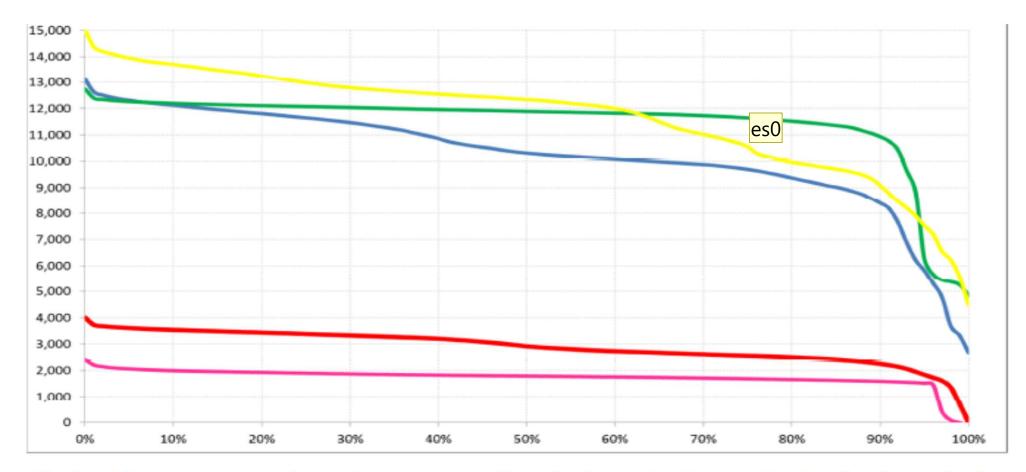


The load durations curves above show one year of hourly electric loads sorted high to low for each of the five sites. The graphs are not 'stacked' so the relative size can be viewed Slide 50

es0 Preliminary sizing starts at 75% edw stoermer, 2021-10-05T18:58:20.423



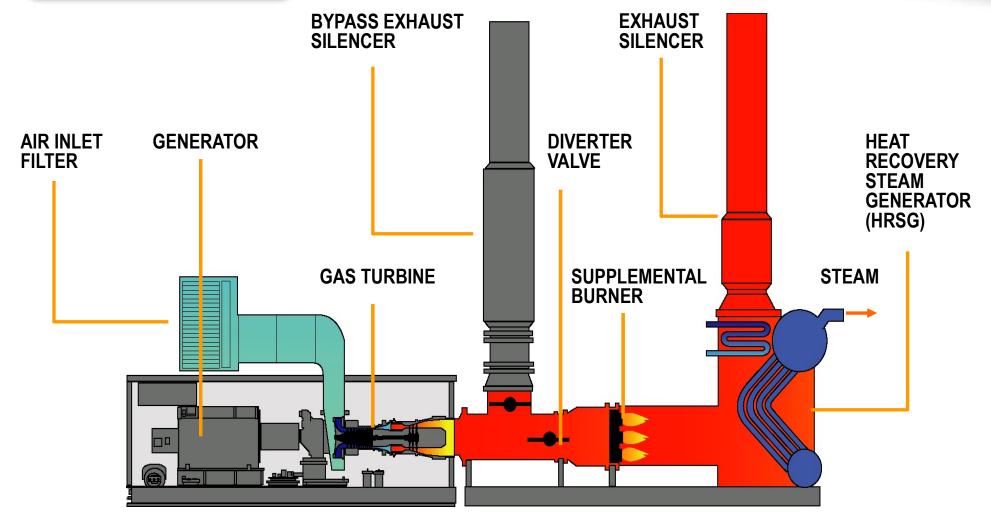
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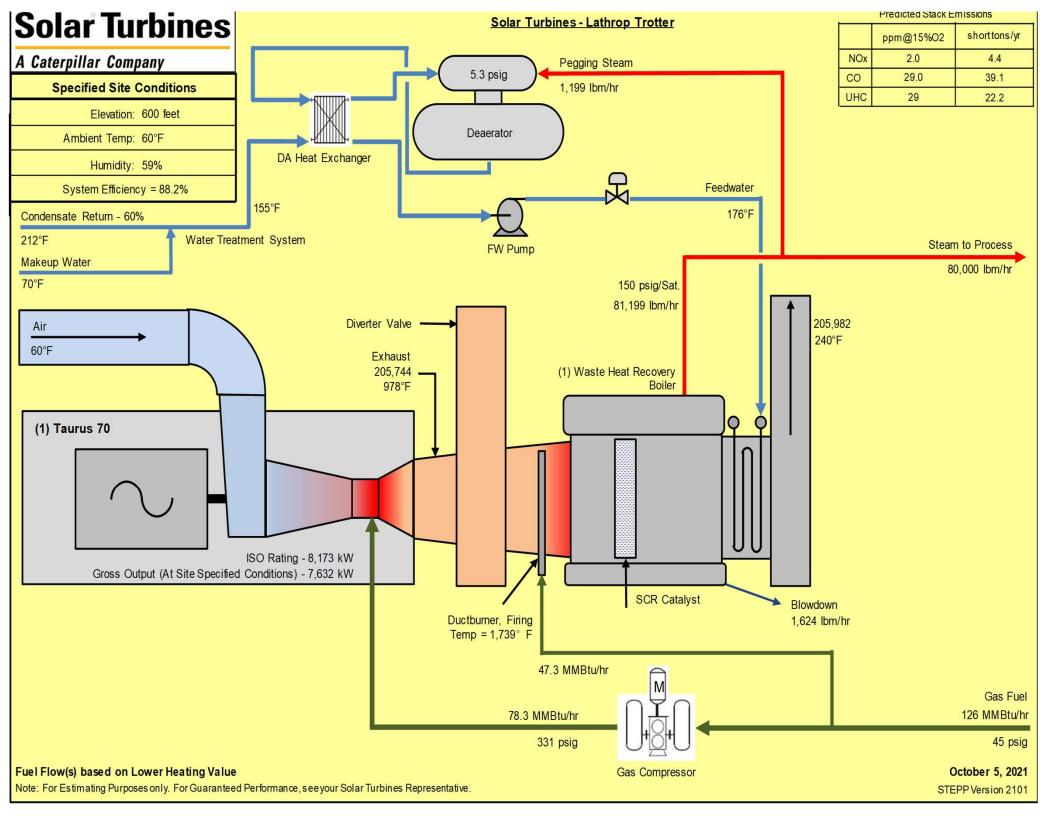
Solar Turbines Engine Performance Program v.1901.0

Customer Name		Lathrop Trotter - Solar Turbines					
Project Name	Sample - Industrial Manufacturing						
Project Location			Ohio, India	na, Kentucky	, Pennsylvani	a	
_							
	Taur						
		Natural Ga	S		selections, an	d access other pro	gram leatures
Dual Fuel or Single Fuel?	Gas Only		•				
	- the second	<u> </u>					
Display selected column's results in o	other sneets	0	0	U	0	U	0
Site Elevation	feet	800	800	800	800	800	800
Ambient Temperature (T1)	°F	-10	32	53	53	68	93
Relative Humidity	%	0	5	20	20	40	70
Barometric Pressure	"Hg	29.1	29.1	29.1	29.1	29.1	29.1
Inlet Duct Loss	"H2O	4.0	4.0	4.0	4.0	4.0	4.0
Exhaust Duct Loss	"H2O	10.0	10.0	10.0	10.0	10.0	10.0
Site Fuel Gas Pressure	psig	36	36	36	36	36	36
Process Steam Pressure	psig	260	260	260	260	260	260
Steam Saturation Temperature	°F	410	410	410	410	410	410
Process Steam Temperature	°F	410	410	410	410	411	411
Steam Flow to Process	lbm/hr	80,000	70,000	56,000	80,000	60,000	50,000
Condensate Temperature	°F	212	212	212	212	212	212
Condensate Return	%	60	60	60	60	60	60
Makeup Water Temperature	°F	60	60	60	60	60	60
	Project Name Project Location Turbine Selected/Modeled Fuel Type Dual Fuel or Single Fuel? Display selected column's results in Display selected column's results in Site Elevation Ambient Temperature (T1) Relative Humidity Barometric Pressure Inlet Duct Loss Exhaust Duct Loss Site Fuel Gas Pressure Process Steam Pressure Steam Saturation Temperature Process Steam Temperature Steam Flow to Process Steam Flow to Process	Project NameProject LocationProject LocationTurbine Selected/ModeledFuel TypeDual Fuel or Single Fuel?Gas OnlyDisplay selected column's results in the sheetsSite ElevationfeetAmbient Temperature (T1)°FRelative Humidity%Barometric Pressure"H2OExhaust Duct Loss"H2OSite Fuel Gas PressurepsigProcess Steam PressurePsigSteam Saturation Temperature°FSteam Flow to ProcessIbm/hrCondensate Return%	Project Name Project LocationTurbine Selected/ModeledTaurus 70-111013Turbine Selected/ModeledTaurus 70-111013Fuel TypeNatural GaDual Fuel or Single Fuel?Gas OnlyDisplay selected column's results in ther sheetsCSite Elevationfeet800Ambient Temperature (T1)°F-10Relative Humidity%0Barometric Pressure"Hg29.1Inlet Duct Loss"H2O4.0Site Fuel Gas Pressurepsig36Process Steam Pressurepsig260Steam Saturation Temperature°F410Process Steam Temperature°F410Steam Flow to ProcessIbm/hr80,000Condensate Temperature°F212Condensate Return%60	Project Name Project LocationSampleProject LocationTurbine Selected/ModeledTaurus 70-11101S AxialTurbine Selected/Modeled Dual Fuel or Single Fuel?Taurus 70-11101S AxialDual Fuel or Single Fuel?Gas OnlyImage: Complement of the selected column's results in the sheetsComplement of the selected column's results in the sheetsDisplay selected column's results in the sheetsComplement of the selected column's results in the sheetsSolutionSite Elevationfeet800800Ambient Temperature (T1)°F-1032Barometric Pressure"Hg29.129.1Inlet Duct Loss"H2O4.04.0Exhaust Duct Loss"H2O10.010.0Site Fuel Gas Pressurepsig3636Process Steam Pressurepsig260260Steam Saturation Temperature°F410410Process Steam Temperature°F410410Or Condensate Temperature°F212212Condensate Return%6060	Project NameSample - Industrial MathematicationProject LocationOhio, Indiana, KentuckyTurbine Selected/ModeledTaurus 70-11101 > AxialFuel TypeNatural GasDual Fuel or Single Fuel?Gas OnlyDisplay selected column's results in ther sheetsCDisplay selected column's results in ther sheetsCSite ElevationfeelRelative Humidity%05Barometric Pressure"Hg29.129.1Site Fuel Gas Pressure"H2OMatural Gas Process Steam Pressurepsig3636Steam Saturation Temperature°F410410AthonProcess Steam Temperature°F410410AthonProcess Steam Temperature°F410410AthonSteam Flow to ProcesBibm/hr80,00070,00056,000Condensate Return%6060	Project Name Project LocationSample - Industrial Maufacturing Ohio, Indiana, Kentucky, PennsylvaniTurbine Selected/Modeled Fuel Type Dual Fuel or Single Fuel?Taurus 70-11101S Axial Gas OnlySee STEPP T selections, and Gas OnlyDisplay selected column's results in the sheetsCCCSee STEPP T selections, and Selections, and Selections, and Gas OnlyDisplay selected column's results in the sheetsCCCSee STEPP T selections, and Selections, and 	Project NameSample - Industrial Manufacturing Ohio, Indiana, Kentucky, PennsylvaniaTurbine Selected/ModeledTaurus 70-11101S Axial Natural Gas Dual Fuel or Single Fuel?See STEPP TOULS tab to select selections, and ceress other process other process Stem PressureDisplay selected column's results in other sheetsOImage: Constraint of the selection of the se

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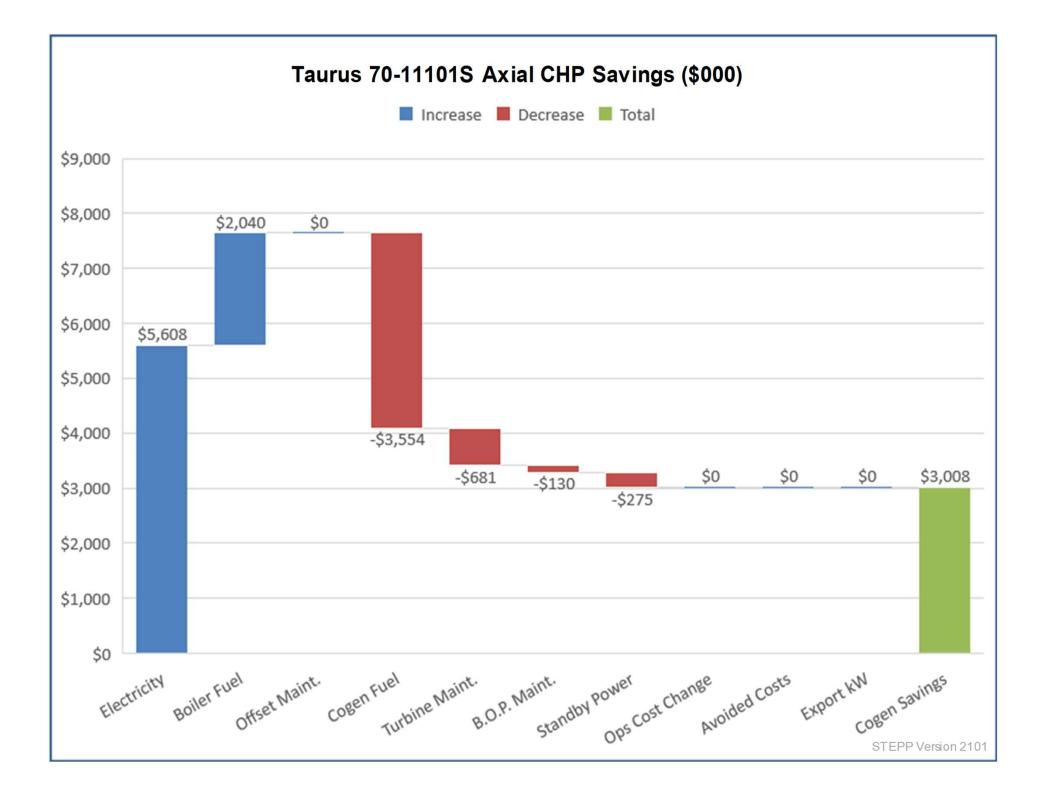


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### **Cogeneration Plant Estimated Performance Summary**

KW Gross Output @ ISO Conditions:	8,170 KW
KW Gross Output @ specified site conditions:	7,632 KW
Net Gas Turbine Power Production:	7,330 KW
Boiler Steam Flow (HRSG design uses 27.0°F pinch, 18.0°F approach):	81,202 lbm/hr
Steam Flow to Process:	80,000 lbm/hr
Cycle Performance (lower heating value basis):	
Solo I offormation (lottor floating value sacio).	
Net Turbine Electrical Heat Rate:	10,680 Btu/kWHR
	10,680 Btu/kWHR <sup>3,870</sup> Btu/kWHR
Net Turbine Electrical Heat Rate:	,



### Annual Savings

Current System Costs:	
Annual Electricity Cost (offset by proposed system):	
7,330 kW x 0.09\$/kW x 8500 hrs/year =	\$5,607,500
Steam Production Costs (fuel and O&M):	
81,199 lbm/hr x 8500 hrs/year x \$3.00/klbm =	\$2,040,000
Current Annual Maintenance Costs to be Offset	\$0
Total Annual Current Costs	\$7,647,500
Proposed Cogeneration System Costs:	
Annual Cogeneration System Fuel Cost:	
125.6 MMBtu/hr x \$3.00/MMBtu x 1.109 HHV/LHV x 8500 hrs/year =	\$3,554,000
Turbine Maintenance Cost (based on gross power output):	
\$0.0105/kW-hr x 7,632 kW x 8500 hrs/year =	\$681,200
Balance of Plant Maintenance Cost (based on gross power output):	
\$0.002/kW-hr x 7,632 kW x 8500 hrs/year =	\$129,800
Standby Power Cost (based on gross power output):	
\$3.00/kW-month x 12 months x 7,632 kW =	\$274,800
Increase/Decrease in Annual Operations Cost	\$0
Avoided Costs, \$/year	\$0
Export KW Revenue, \$/year	\$0
Total Annual Proposed Costs	\$4,639,800

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# Evaluating CHP Emission Impacts

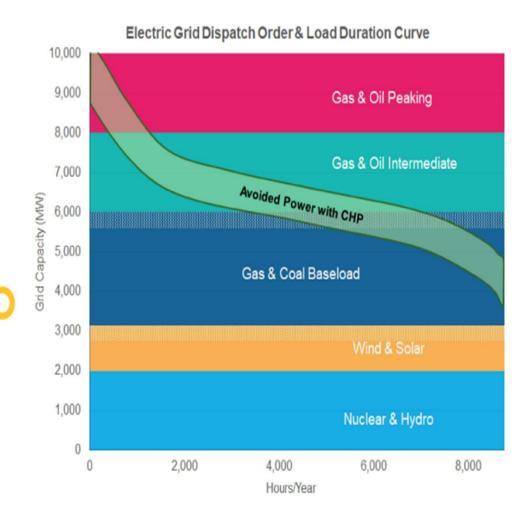
# Displaced grid emissions for CHP are based on *marginal utility generation*

Marginal units are those at the "top of the stack" that set the electricity price in real-time or dayahead pricing

Currently, marginal generation tends to be provided by units fueled by gas, oil, and in some cases coal

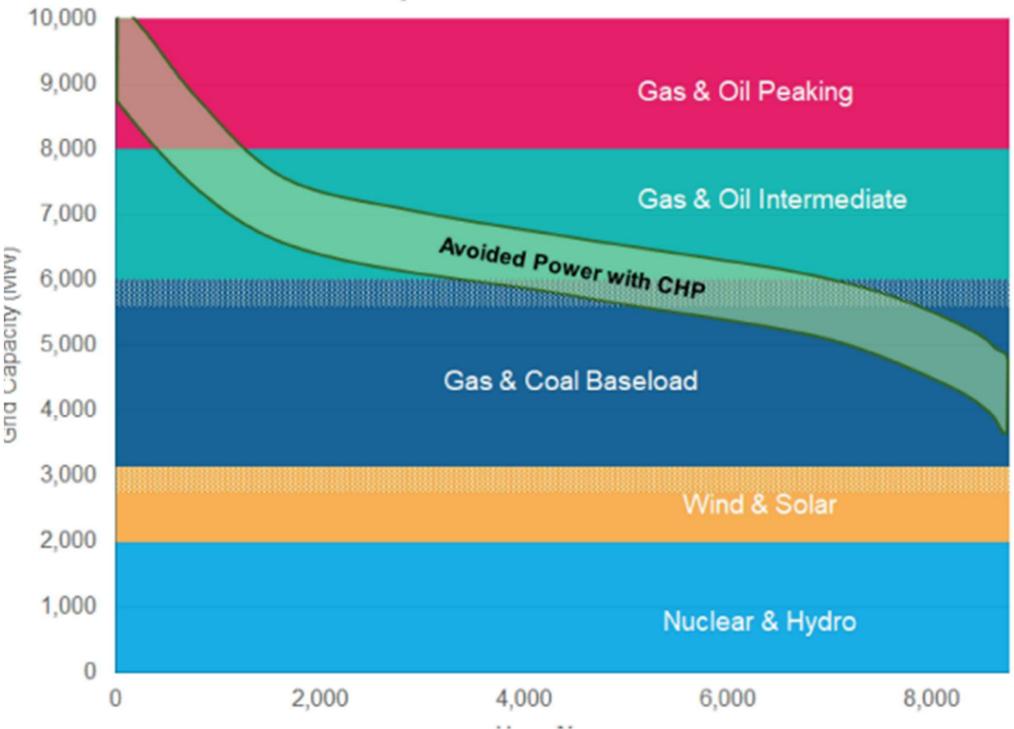
- For CHP systems that operate 24/7, average fossil fuel emission factors from eGRID can be used
- For CHP systems that operate during day/evening hours, average non-baseload emission factors from eGRID provide a better estimate

Limitations in accurately estimating marginal emissions with eGRID





### Electric Grid Dispatch Order & Load Duration Curve









The results generated by the CHP Emissions Calculator are intended for educational and outreach purposes only; it is not designed for use in developing emission inventories or preparing air permit applications.

Annual Emissions Analysis					
	CHP System	Displaced Electricity Production	Displaced Thermal Production	Emissions/Fuel Reduction	Percent Reduction
NOx (tons/year)	43.51	78.92	44.50	79.90	65%
SO2 (tons/year)	1.66	150.70	0.22	149.27	99%
CO2 (metric tons/year)	83,973	112,520	48,035	76,583	48%
Carbon (metric tons/vear)	22,902	30.687	13,100	20.886	48%
Fuel Consumption (MMBtu/year)	1,555,699	1,341,814	889,908	676,023	30%
Acres of Forest Equivalent				20,886	
Number of Cars Removed				13,054	

Displaced Electricity Generation Profile: eGRID State Average Fossil 2016

**Region Selected: Ohio** 

This reduction is equal to removing the carbon that would be absorbed by 20,886 acres of forest

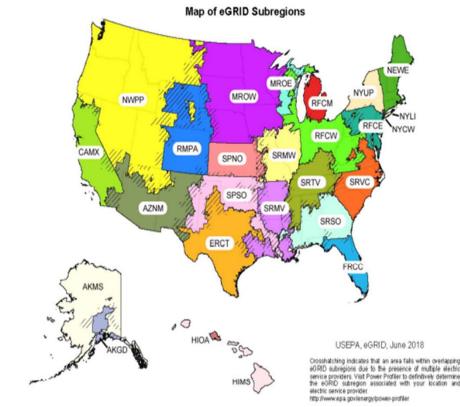


This reduction is equal to removing the carbon emissions from 13,054 cars



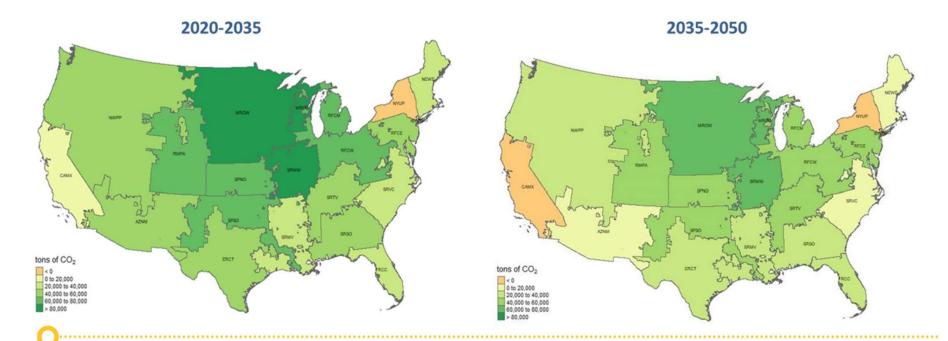
# Estimating Future Emissions by eGRID Subregion

The subregion emission rates most accurately represent the actual electricity used by consumers by limiting the import and export of electricity within an aggregated area.





## CHP REDUCES CARBON EMISSIONS **DRASTICALY** USING NATURAL GAS & REACHES ZERO EMISSIONS ON RNG & GREEN H2



## Lifetime Carbon Emission Reductions for CHP Systems



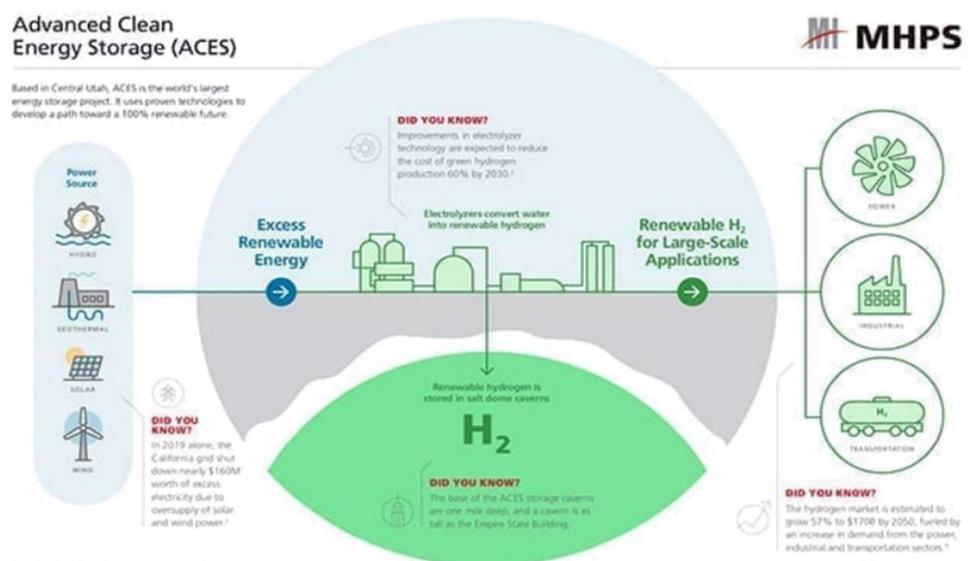
Category	10 MW CHP	10 MW WHP	10 MW PV	10 MW Wind	10 MW NGCC
Annual Capacity Factor	85%	85%	24.9%	35.5%	57.6%
Annual Electricity, MWh	74,460	74,460	21,812	31,098	50,458
Annual Useful Heat Provided, MWh <sub>th</sub>	97,505	None	None	None	None
Capital Cost, \$ million	\$20.2 m	\$15.0 m	\$17.8 m	\$16.2 m	\$10.0 m
Annual Energy Savings, MMBtu	360,420	787,597	230,720	328,938	200,693
Annual CO <sub>2</sub> Savings, Tons	53,297	78,265	22,927	32,687	33,571
Annual NOx Savings, Tons	45.4	39.6	14.5	20.7	32.0

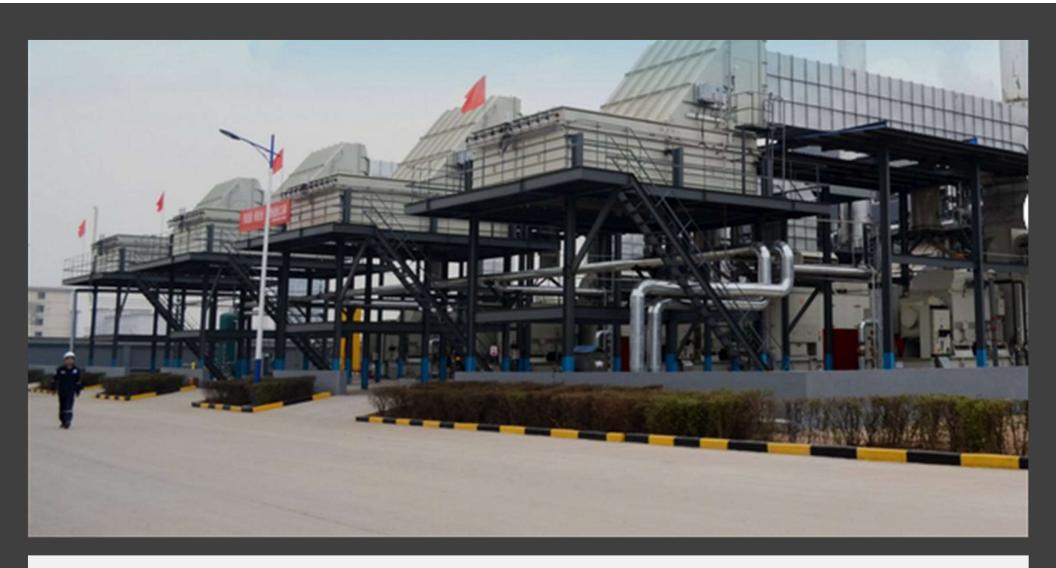
CHP's Higher Efficiency Results in Energy and Emissions Savings Compared to Today's Grid (Average Fossil Generation)



# **GREEN HYDROGEN**

### A KEY FACTOR IN REACHING ZERO EMISSIONS WITH CHP





High Hydrogen Titan – 130 Units burn 50% H2  AS RENEWABLE NATURAL GAS & GREEN HYDROGEN BECOME READILY AVAILIABLE, SOLAR GT'S CAN ACCEPT THAT AS A FUEL AND BE ZERO EMISSIONS !!





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The recently passed IRA increased the ITC to 30% (was 10%) if certain provisions could be met.

- Must meet the Prevailing Wage and Apprenticeship levels. This includes construction and repairs for the first 5 years of op.
- 2. Must be started by the end of 2024.
- **3.** Must meet 60% efficiency wouldn't be a problem for CHP.





- NEW: the tax credits are fully fungible. Meaning that you can sell the tax credit to another party. So if the end user's annual tax liability is less than the total of the tax credit, then:
- End user can either roll the remaining tax credit to the following year(s) or
- End user can sell the tax credit to another company who may want them.





2. Must be started by the end of 2024 with a 5% spend by 12-31-24.

If your facility is considering Infrastructure up grades: Boilers, Chillers, Electrical, then the project economics improve even further due to a possible "cost avoidance" by not having to upgrade infrastructure.



# • 30% ITC

Should be attainable provided you met prevailing wages and in some cases that may not be an issue given how hard it is to find people – need to pay more.



# 40% for 100% Made in America

- Lathrop Trotter CHP Preferred Component Suppliers: ALL MADE IN USA
- Solar Gas Turbines: Manufactured in San Diego California
- **Rentech Boilers**: Manufactured in Abilene TX
- Industrial Steam Deaerators: Chicago IL & Iowa



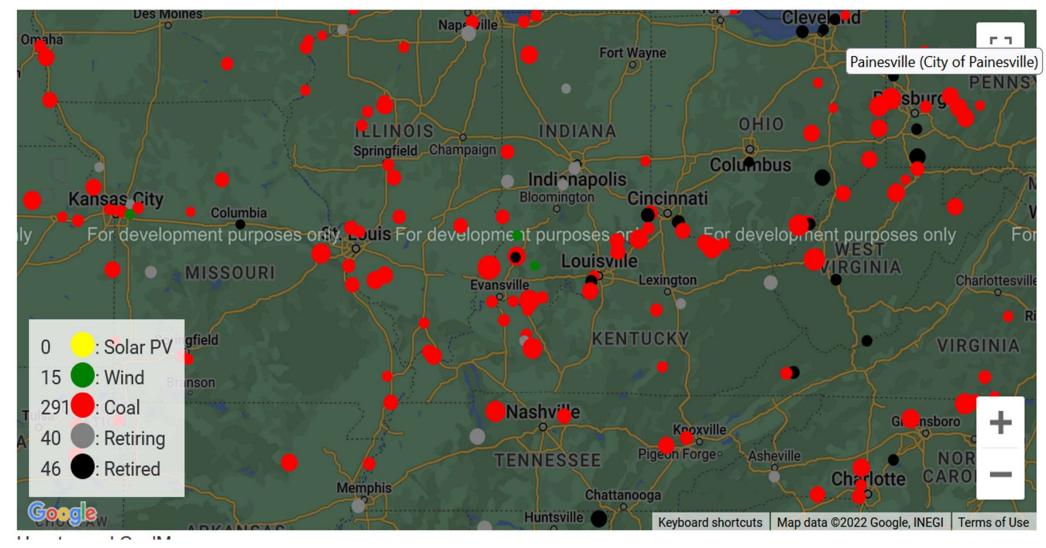
# • 50% ITC

• For projects going into areas where coal fired plants have or will be taken off line and coal mines closed or will be closing.



### COALMAP

Mapping the Economics of U.S. Coal Power and the Rise of Renewables





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## WHAT MAKES CHP WORK ?

- **1.** Economics of Heat Recovery that replaces purchased fuel.
- 2. Economically Viable Pathway to Zero for **Sustainability Goals**
- 3. More **Predictable** Energy Costs.
- 4. Improved **Reliability** Power and Heat.
- 5. Avoided Costs should be considered.
- 6. Teamwork and Experience.
- 7. TAX INCENTIVES VIA IRA





# LATHROP TROTTER Manufacturers Representatives

- Gas Turbines (2-25MW): Solar Turbines
- Heat Recovery & Waste Hreat Boilers: Superior Boiler Works
- Gas Compressors: Vilter / Emerson / Copeland
- Deaerators and Feed Water Equipment: Industrial Steam
- Steam Turbine Gen Sets: Dresser-Rand / Siemens (<300MW)



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# Thank you. Are there any questions?

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### **Biographical Information**



#### Ed Stoermer Cogen and CHP System Sales Engineer

Ed graduated from the University of Cincinnati with a B.S. in Mechanical Engineering and a minor in Business Administration. He later added an Executive Master of Business Administration from Xavier University.

Ed's primary focus is the design and application of combined heat and power systems, using gas and steam turbine generators with heat recovery steam boilers (1-200MW) to help industrial clients

improve their plant's reliability and reduce overall emissions. The ultimate goal is to achieve sustainability goals while simultaneously improving the plant's bottom line profitability through improved energy efficiency. Current projects include refinery power and steam systems, standby power for data centers, specialty fuels, large central steam boilers, and complete steam plant upgrades for healthcare facilities.

In 1999, Ed merged the Stoermer Equipment Company with the RG Anderson Company to form Stoermer-Anderson Inc., a manufacturers rep firm, later selling this to the partners in 2007.

Ed currently lives in Northwest Montana but spends much time in the Midwest to work on power, steam, and special projects. He supports Lathrop Trotter with consulting and training for internal staff and clients and provides expertise in applying gas and steam turbines, boilers, burners, and the balance of plant systems. Ed has been involved in over 400 MWe of CHP projects since he joined the team in 2012.

In his free time, he enjoys backcountry biking, hunting, fishing, and wilderness adventures on horseback and hiking with family and friends.